

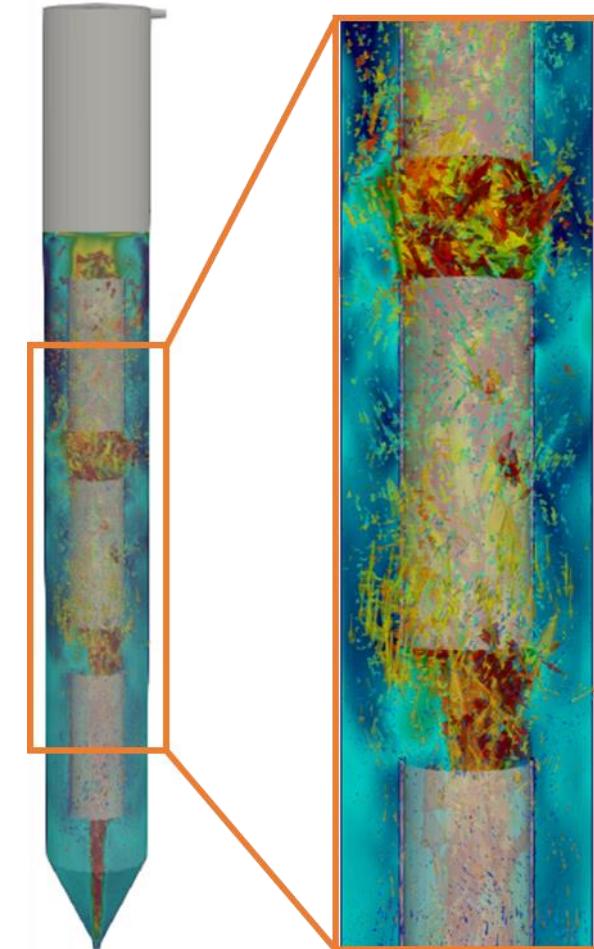
Modelling of Multi-Stage Internal Loop Air Lift Bioreactor Utilizing Computational Fluid Dynamics

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Content

Introduction

- AgRefine project
- Transition to the circular bioeconomy
- Previous works on air lift reactors

Simulation

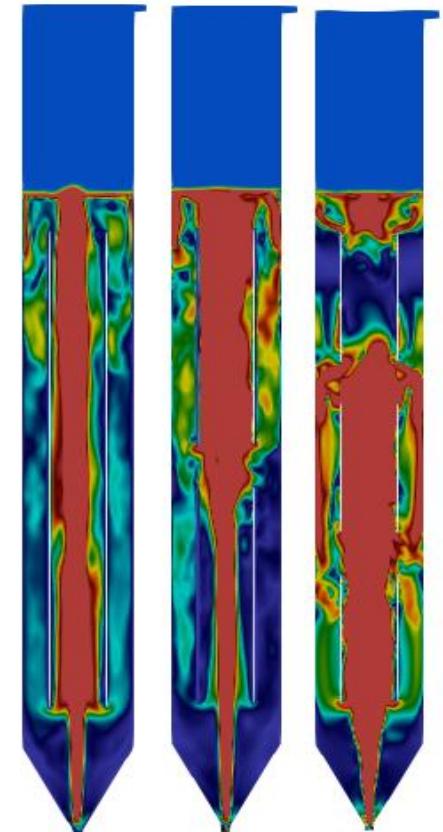
- Reactor geometries in this study
- Simulation set up

Results

- Flow visualization
- Obtained results
- Comparison of upcomer and downcomer velocity

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- Conclusions and future research



About AgRefine – European Training Network

- Green biorefineries
- 15 PhD students, interdisciplinary projects
- 3 work packages



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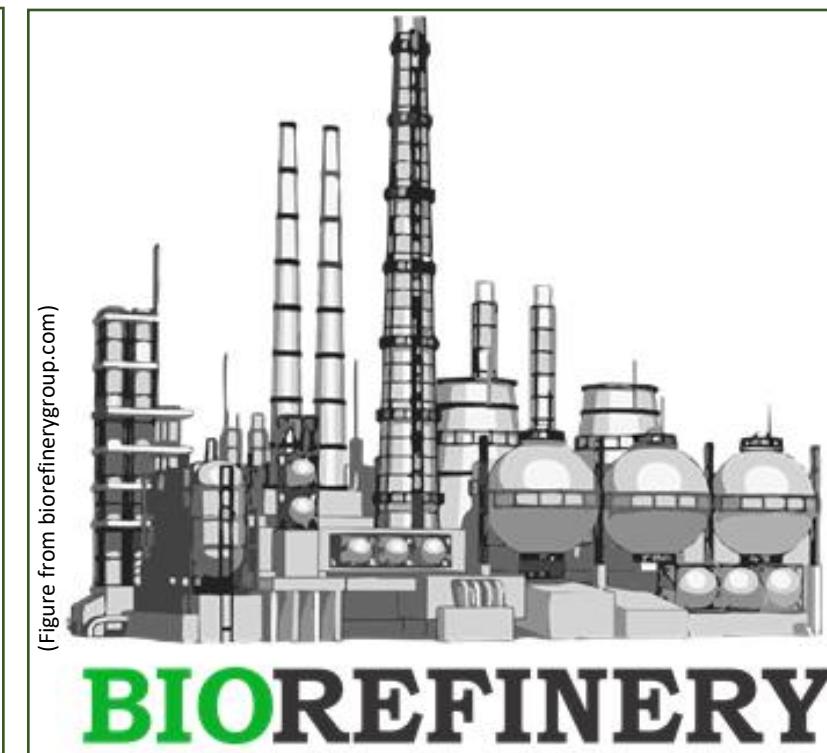
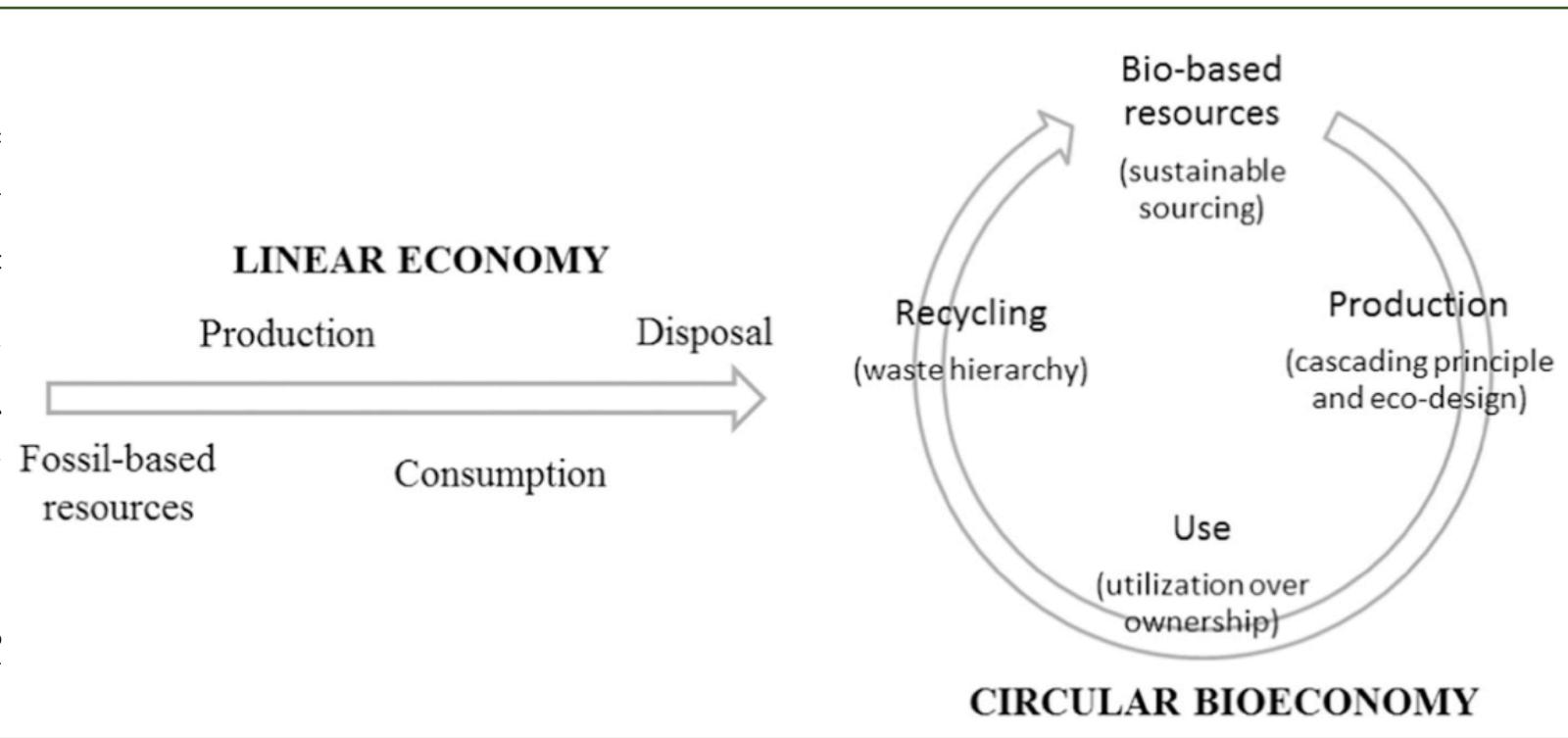


Enviroeye



Transition to the circular bioeconomy

(Figure from D'Amato, Veijonaho, and Toppinen (2020))



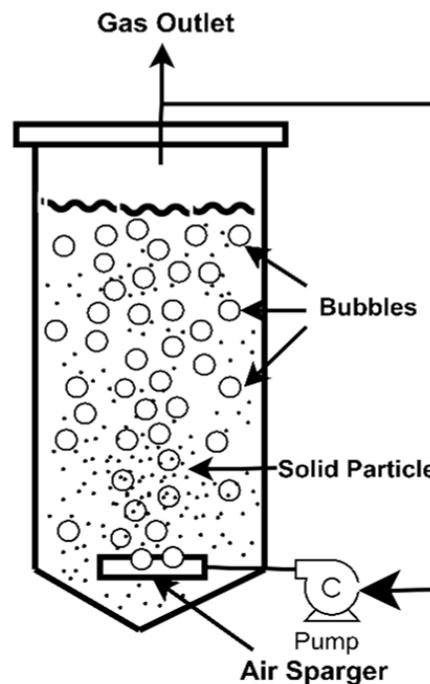
Reactor types

Mechanically stirred

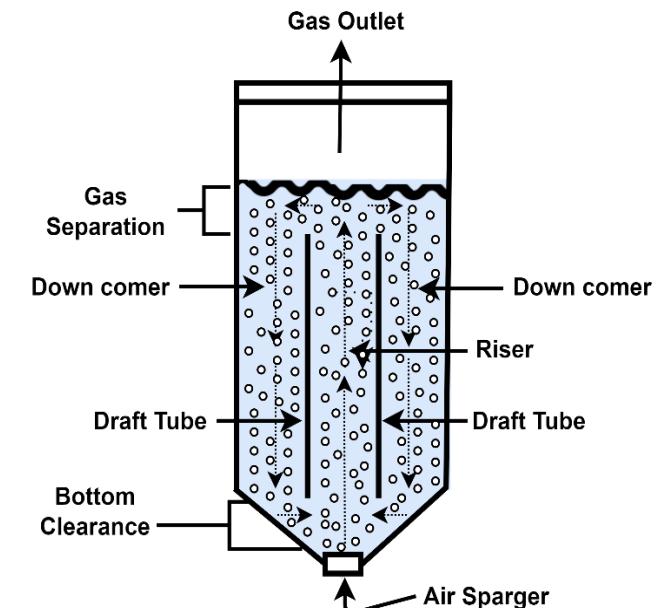


Continuously stirred tank reactor

Pneumatically stirred



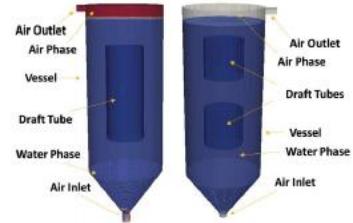
Bubble column



Air lift reactor

My works on ALRs

2021

EU Project Report

CFD optimisation and analysis of existing Anaerobic Digestion and Biorefineries Report

2021

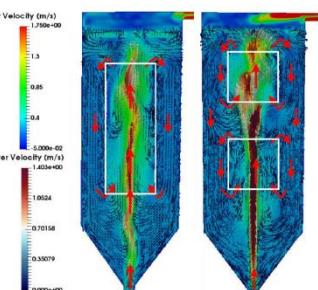
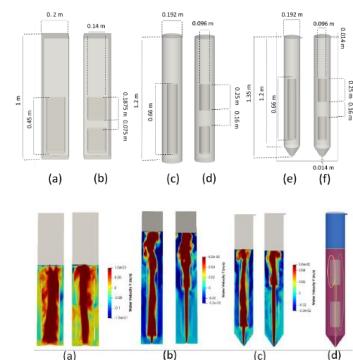
Poster Vienna SS

Figure 2. Flow pattern generated by both geometries.

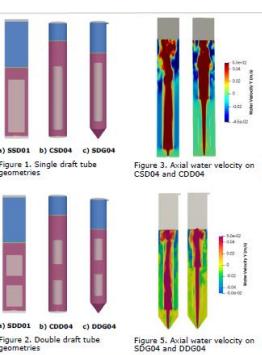
CFD simulation of flow inside air lift bioreactors

2022

PRES22 Conference

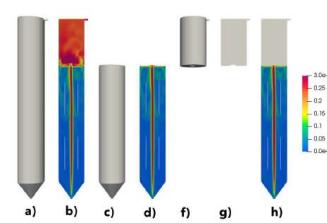
Modelling and Design of Optimal Internal Loop Air-Lift Reactor Configurations Through CFD

2022

Poster Gent

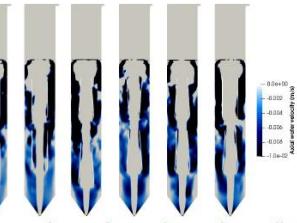
Modelling And Characterization Of Internal Loop Air Lift Bioreactor Configurations Through CFD

2023

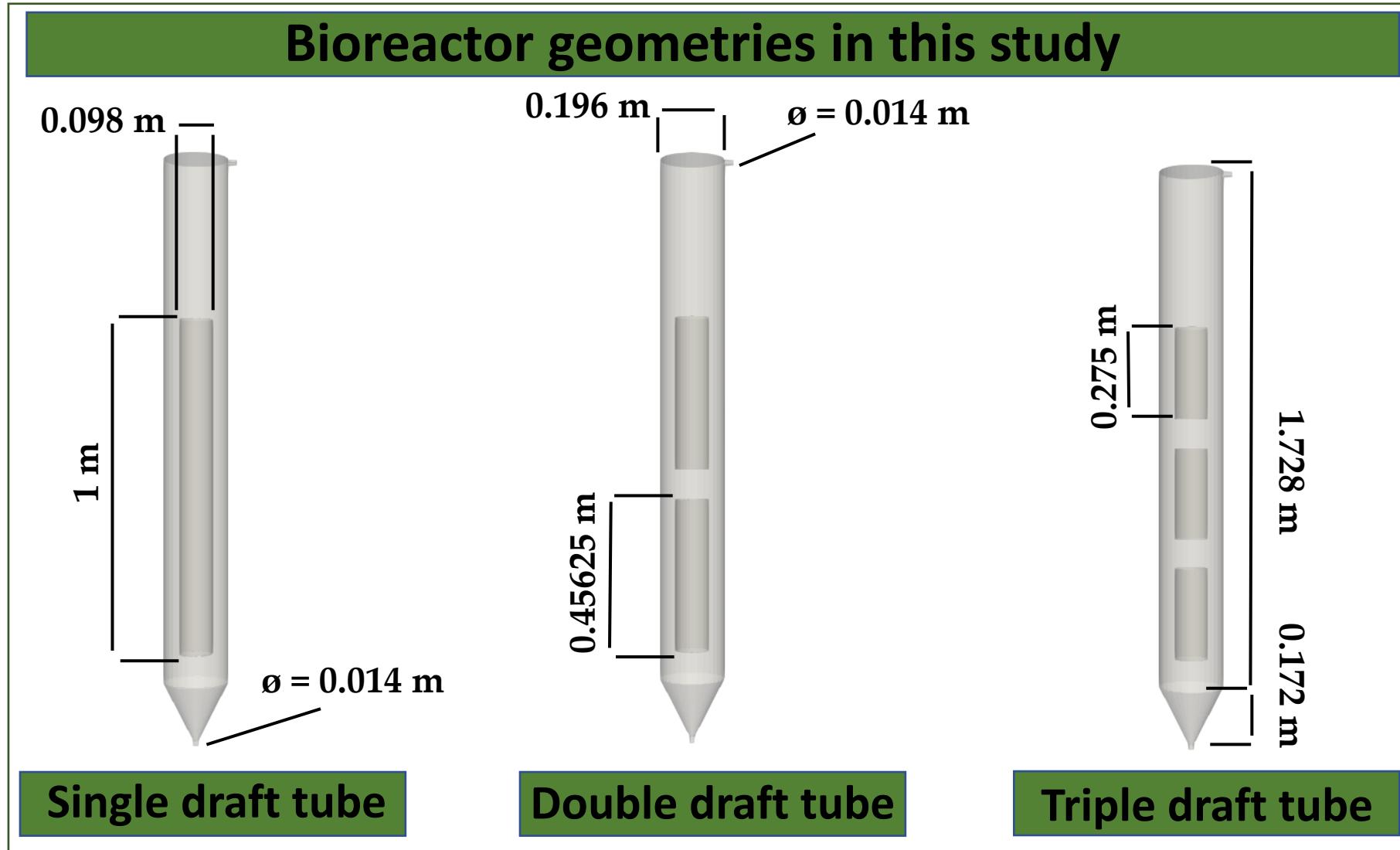
EU Project Report

Geometry and CFD results for Anaerobic Digestion retrofit and Three Phase Bioreactor up-scaling Report

2023

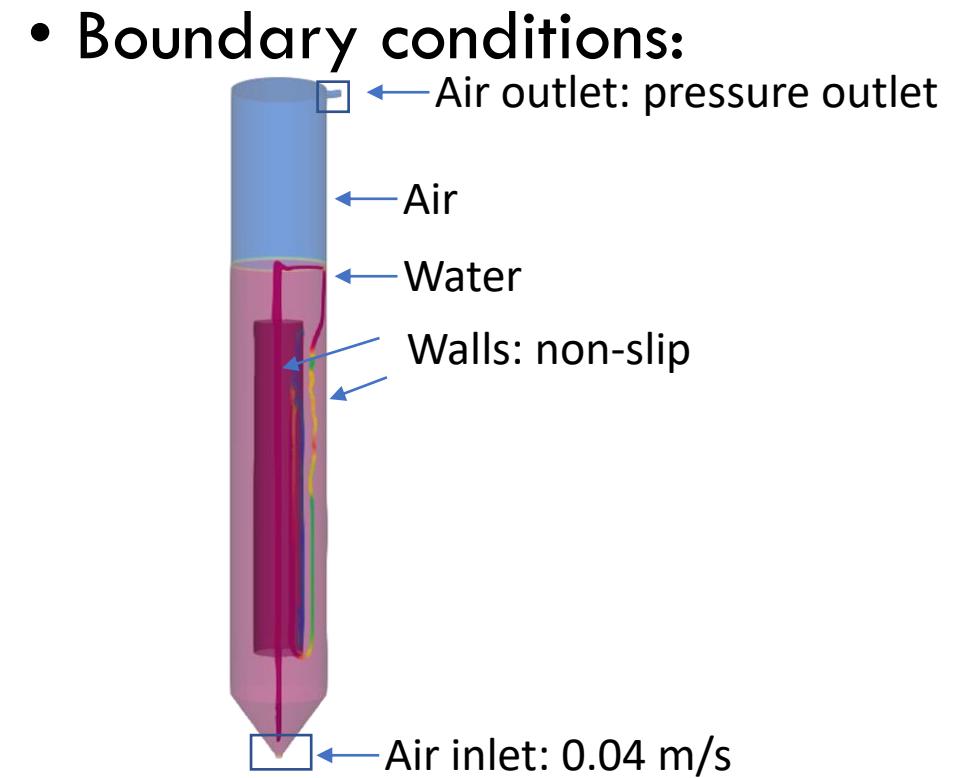
Energies MDPI

Optimal Design of Double Stage Internal Loop Air-Lift Bioreactor

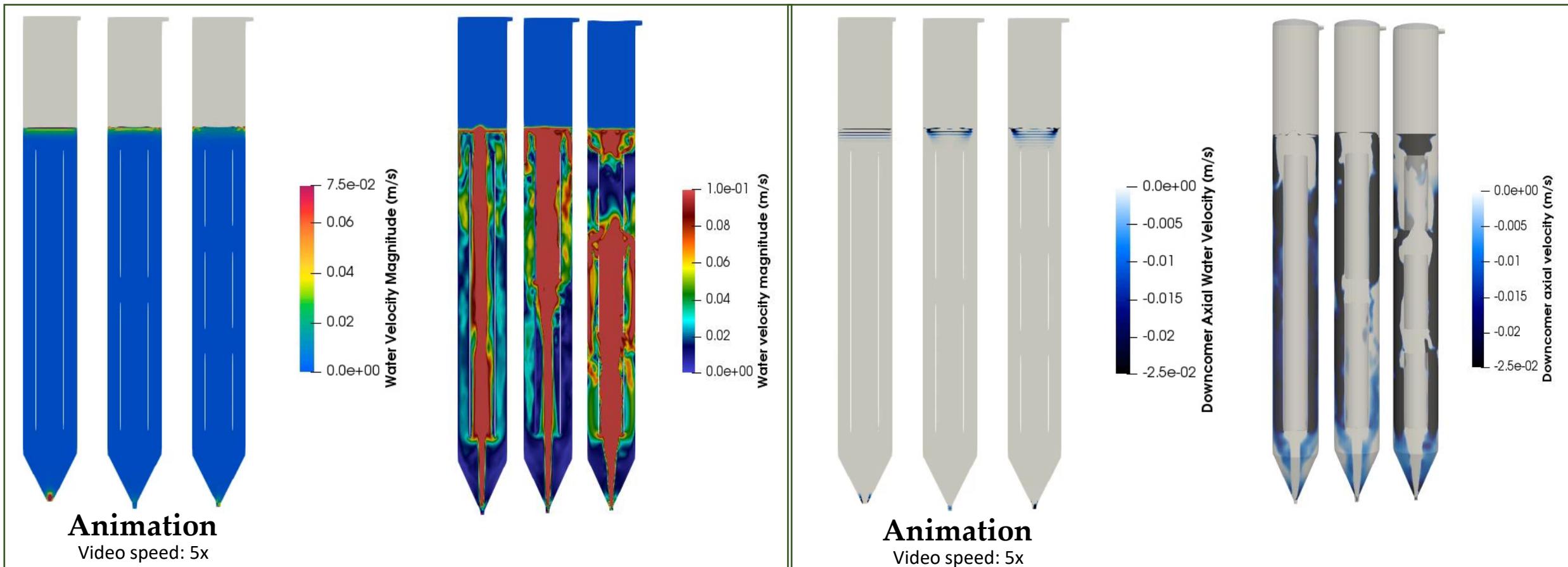


Simulation set up

- Software: OpenFOAM version 9
- Solver: multiphaseEulerFoam
- Mesh:
 - ✓ Cells: ~370,000, ~900,000, ~1,200,000
- Eulerian phase size distribution:
 - Water: 1 mm
 - Air: 4.5 mm

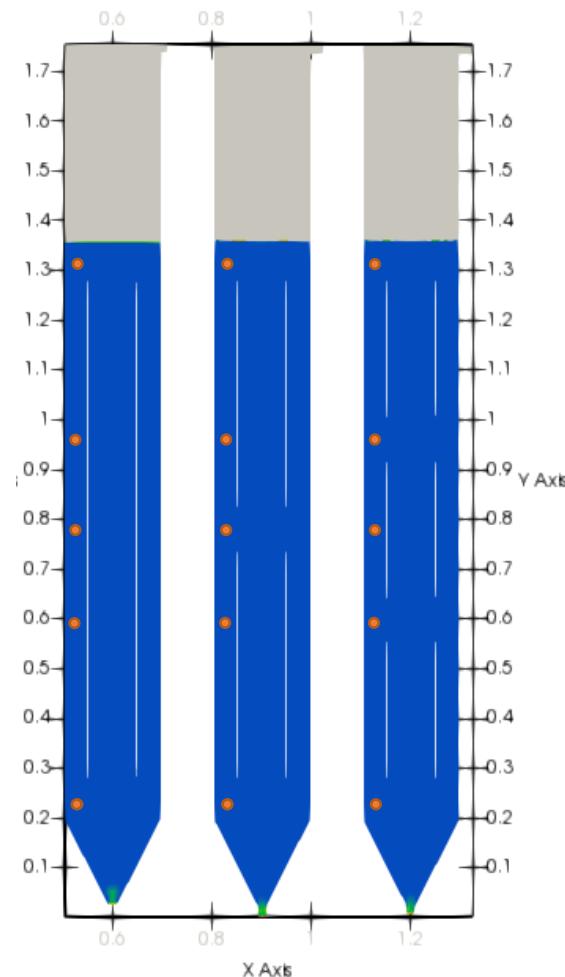


Water velocity comparison



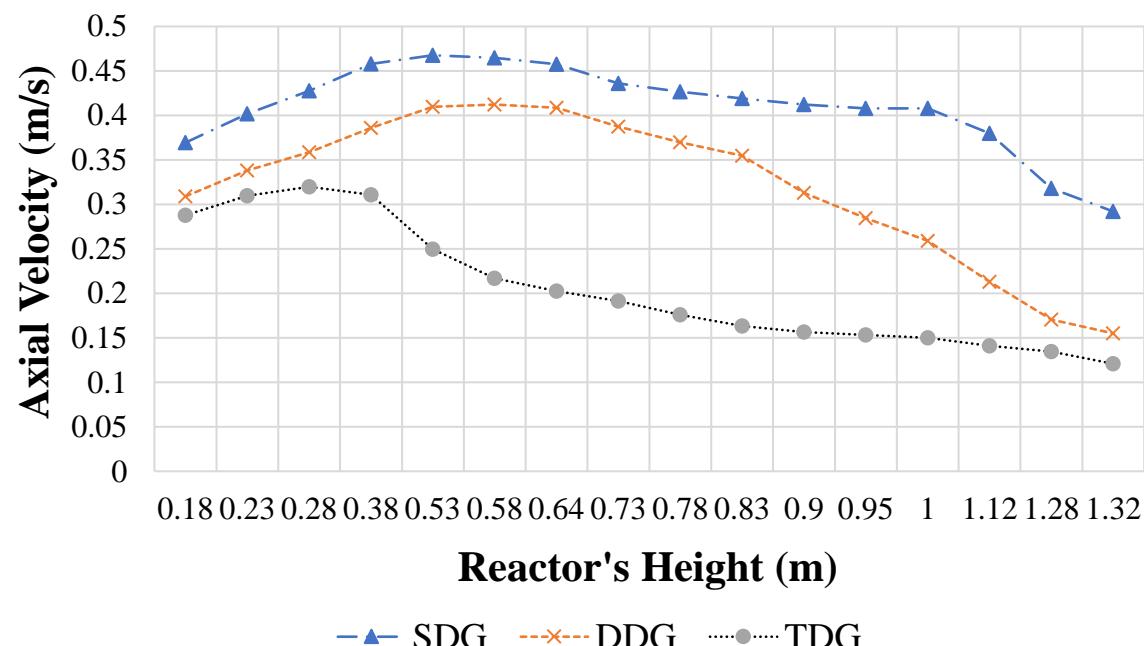
Obtained results

	Pressure (Pa)			Turbulent kinetic energy in fluid phase ($\times 10^{-6} \text{ m}^2/\text{s}^2$)			Fluid velocity on Y-axis ($\times 10^{-2} \text{ m/s}$)		
Height	SDG	DDG	TDG	SDG	DDG	TDG	SDG	DDG	TDG
0.23	111,044	111,048	111,098	3.949	0.999	1.468	0.858	0.121	0.342
0.58	107,623	107,626	107,676	2.792	5.019	9.666	3.497	1.475	1.874
0.78	105,668	105,671	105,721	4.382	16.568	11.175	3.217	2.463	4.086
0.95	104,006	104,009	104,058	7.774	9.551	71.622	3.015	3.987	4.552
1.32	100,386	100,389	100,440	108.579	109.766	113.069	2.647	2.638	2.580

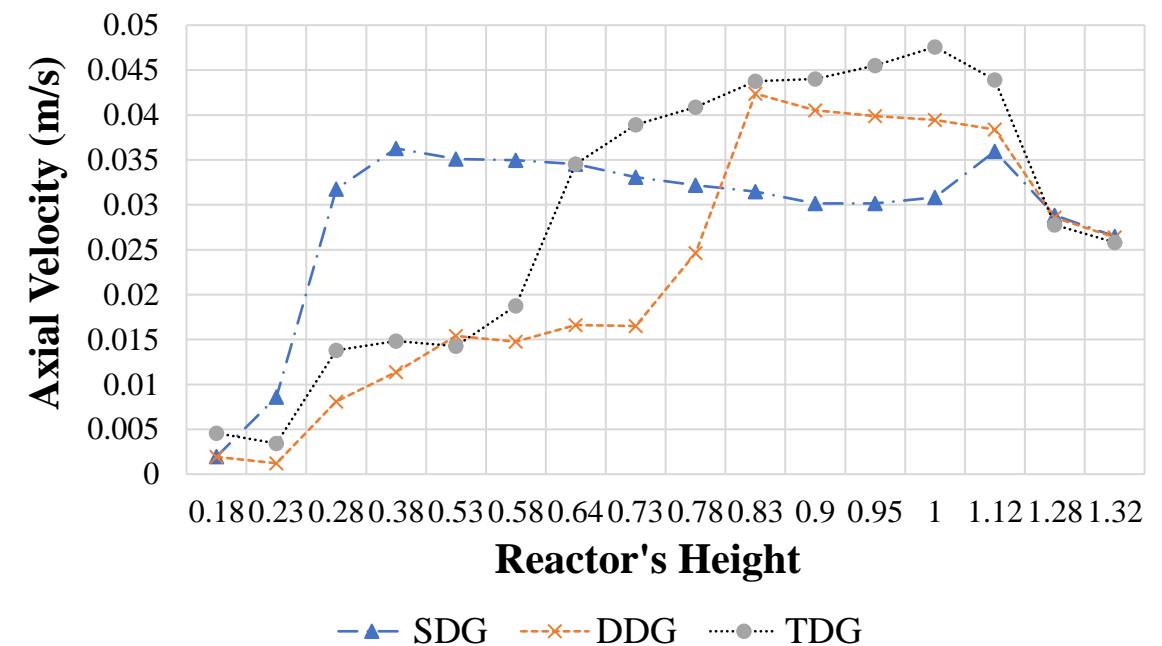


Bioreactors velocity comparison

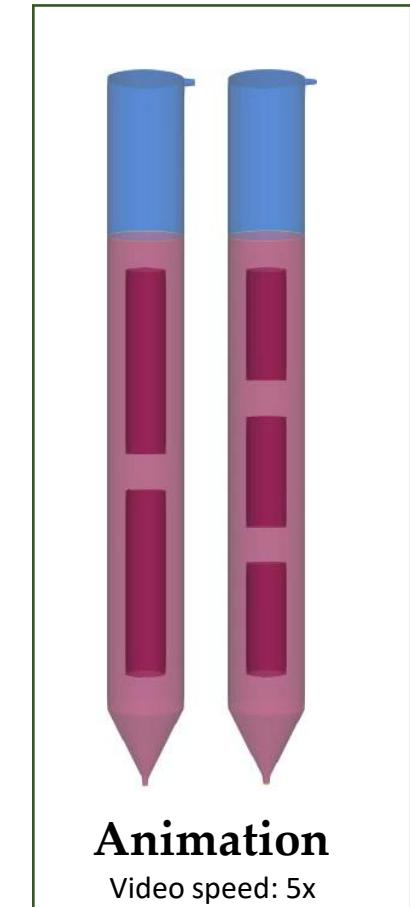
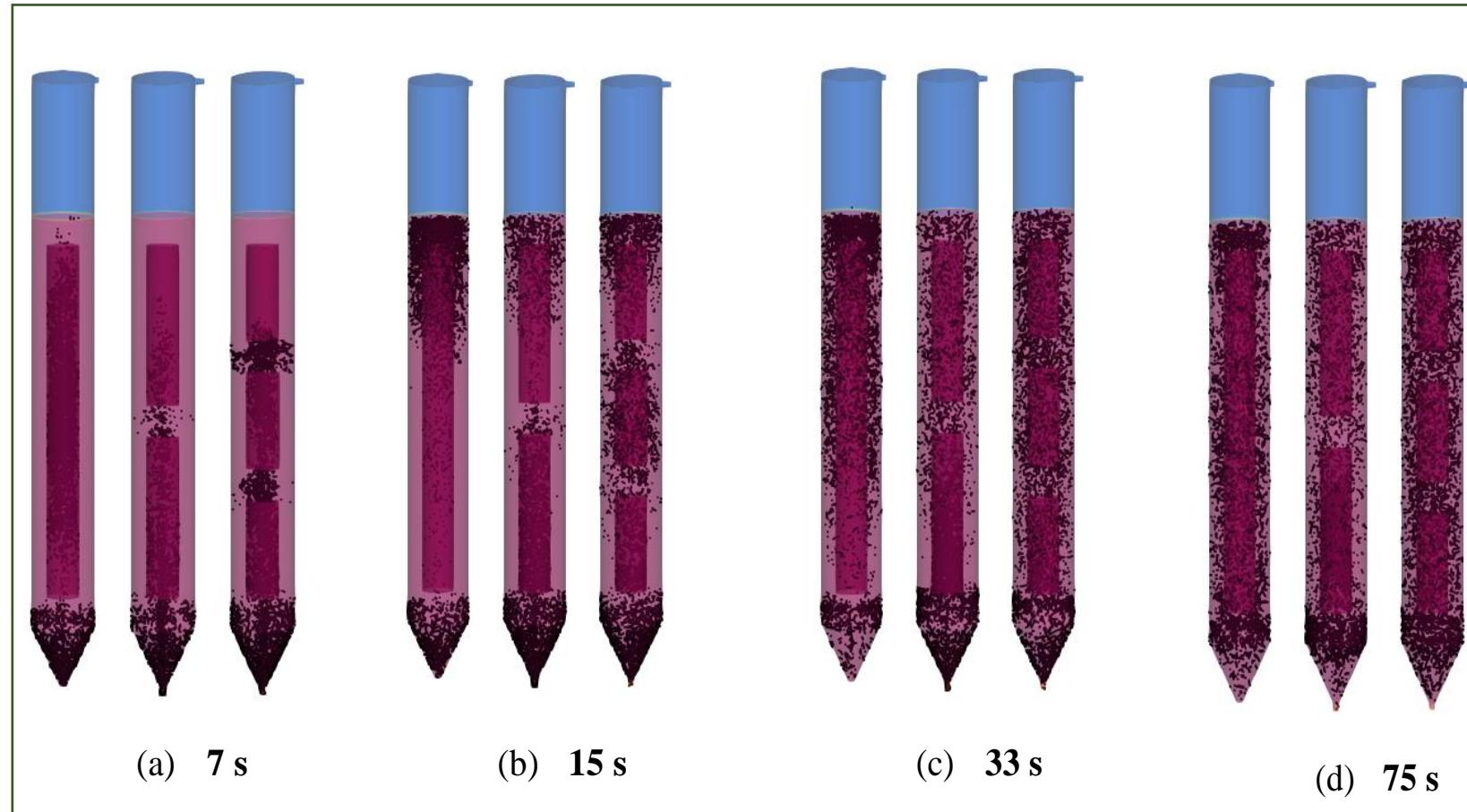
Riser velocity



Downcomer velocity

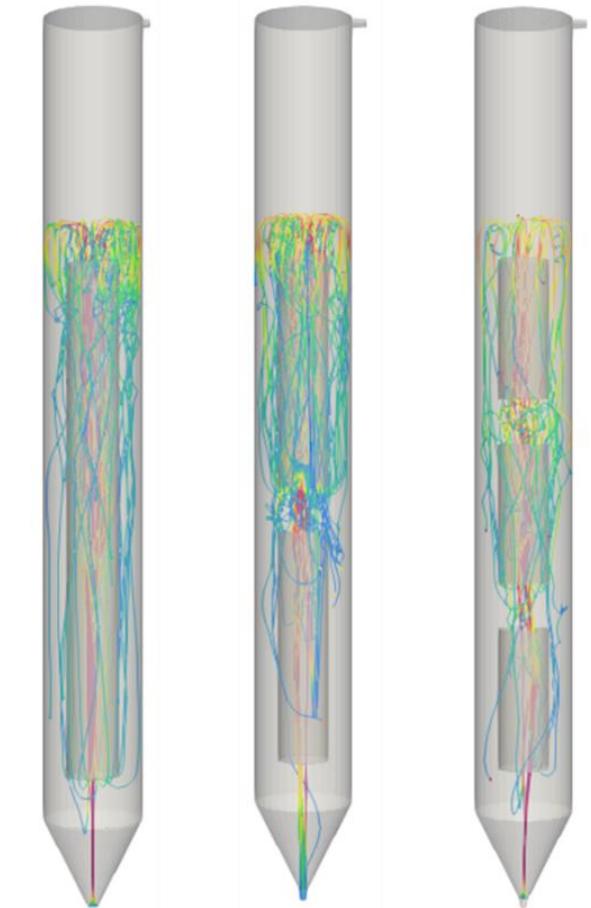


Lagrangian Particles Coupling



Conclusions

- This study compared the hydrodynamics of three different internal loop reactors including multi-stage geometries using CFD simulations.
- The single draft tube geometry maintained a constant downcomer velocity, while the double-stage and triple-stage geometries showed higher downcomer velocities on the top section and a more stable downcomer velocity.
- Particle tracking simulations revealed that the conical bottom is a low fluid circulation zone that can cause the accumulation of solids.
- Coupling Lagrangian particles to the continuous phase of an Euler-Euler simulation allowed for better flow visualization, showing flow and circulation loops.



17th Minisymposium Verfahrenstechnik

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