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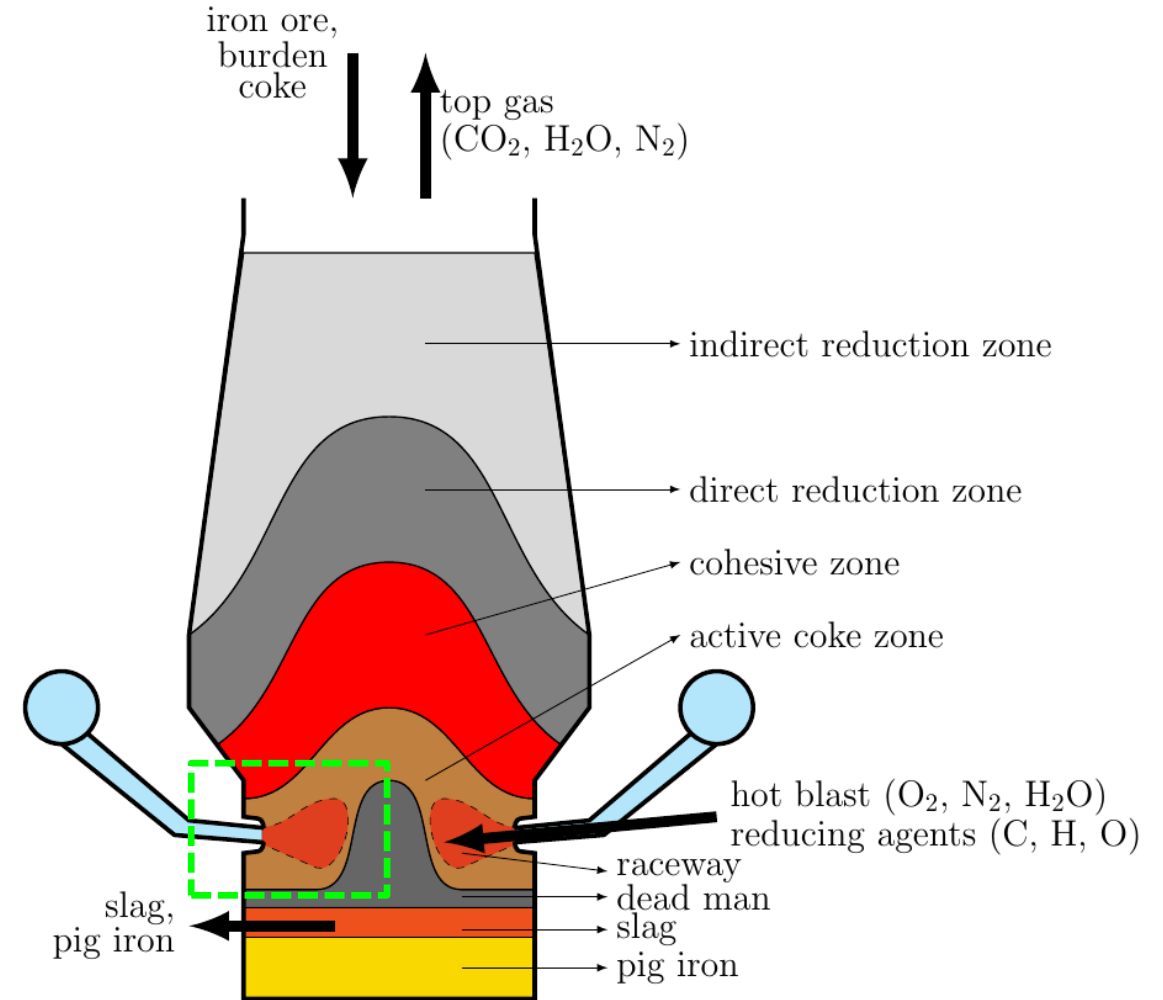
Thermochemical Modeling of the Blast Furnace Raceway Zone

Markus Bösenhofer, Eva-Maria Wartha, Matthias Kiss, Michael Harasek

What is the raceway zone?

- Cavity next to tuyeres

Why is the raceway zone important?



Schematic overview blast furnace process.

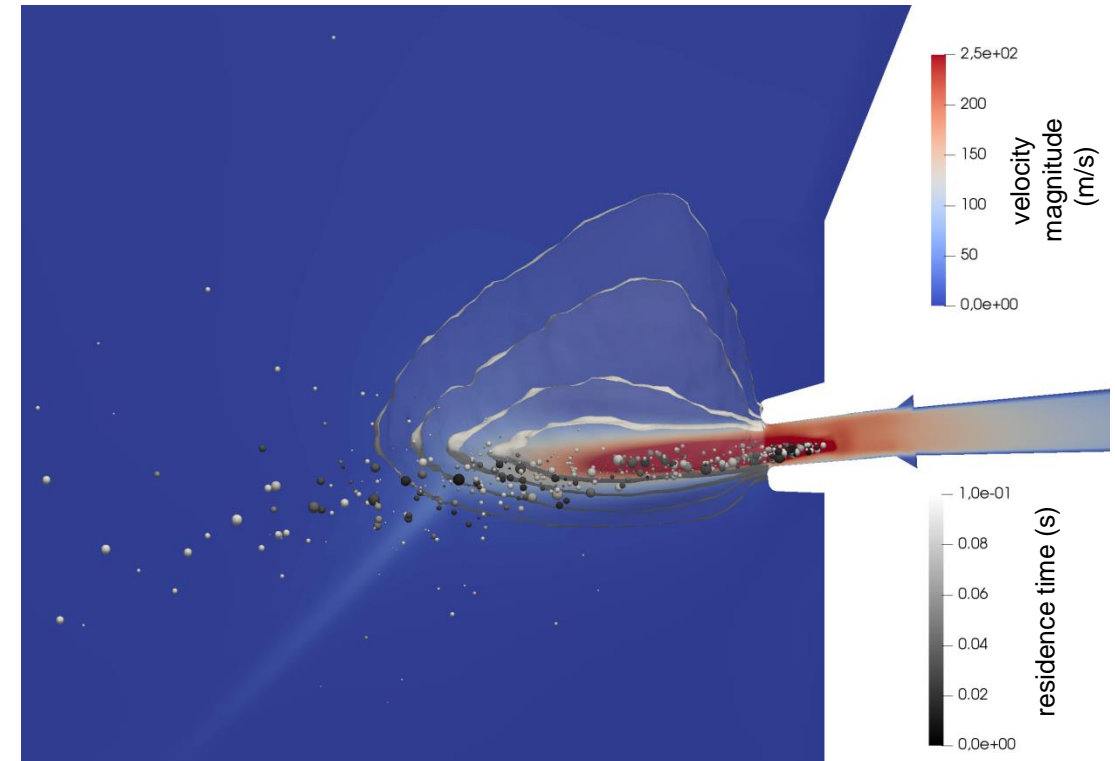


What is the raceway zone?

- Cavity next to tuyeres

Why is the raceway zone important?

- Thermochemical processes influence efficiency
- Injection alternative reducing agents (ARAs)
- Reduction of metallurgical coke consumption

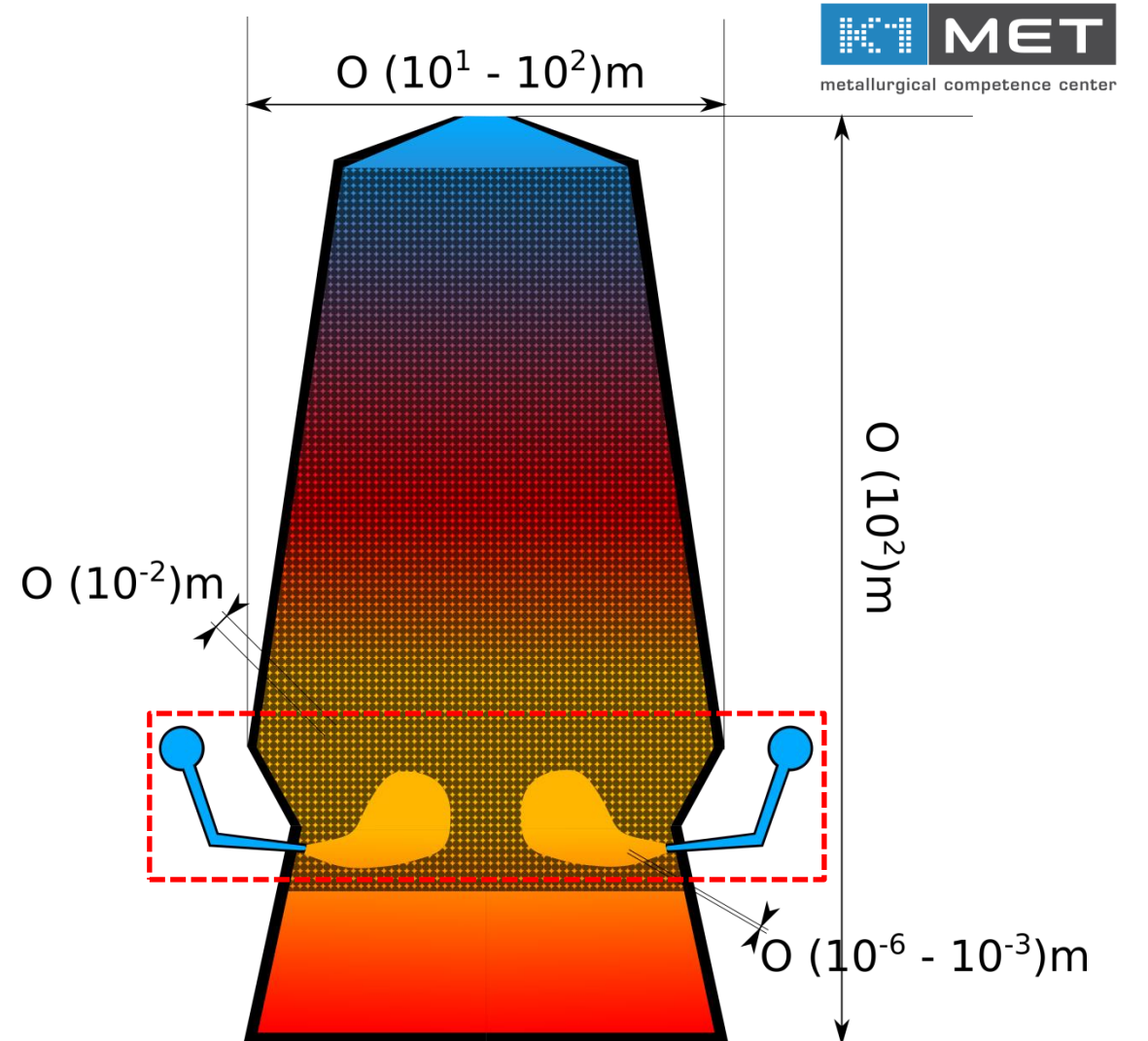


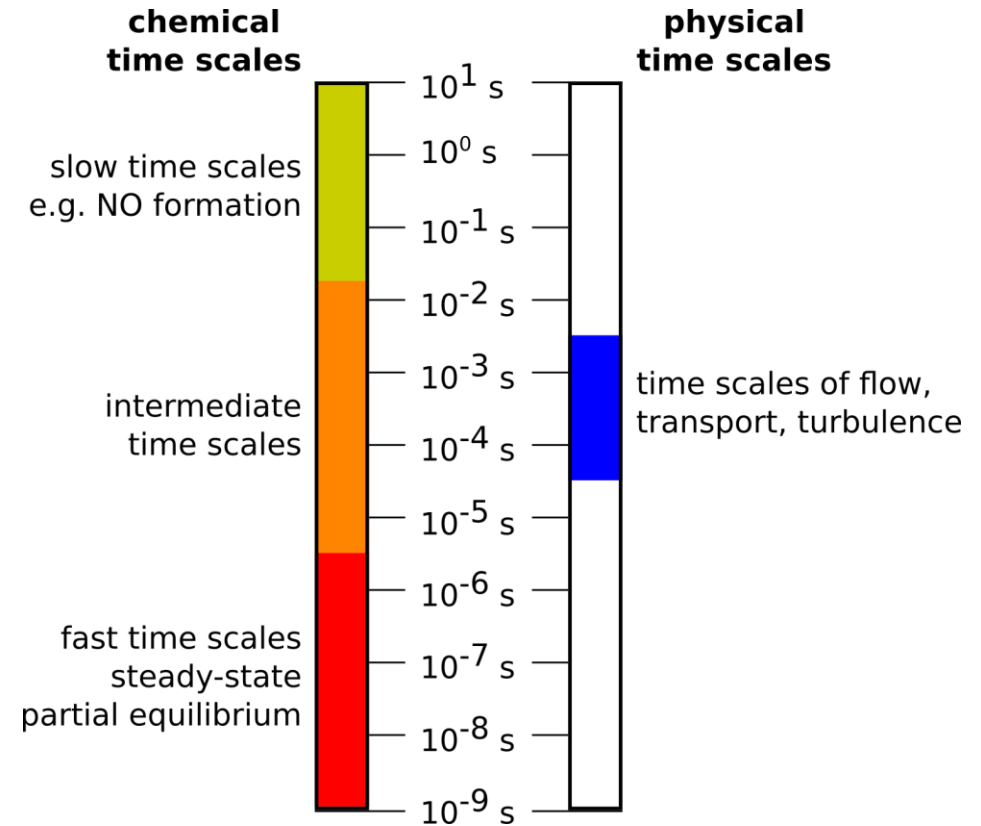
Hot blast velocity and PCI residence time in the raceway zone.

Involved Length Scales

Geometrical scales

- Blast furnace size
- Coke/Ore/Aggregates
- ARAs





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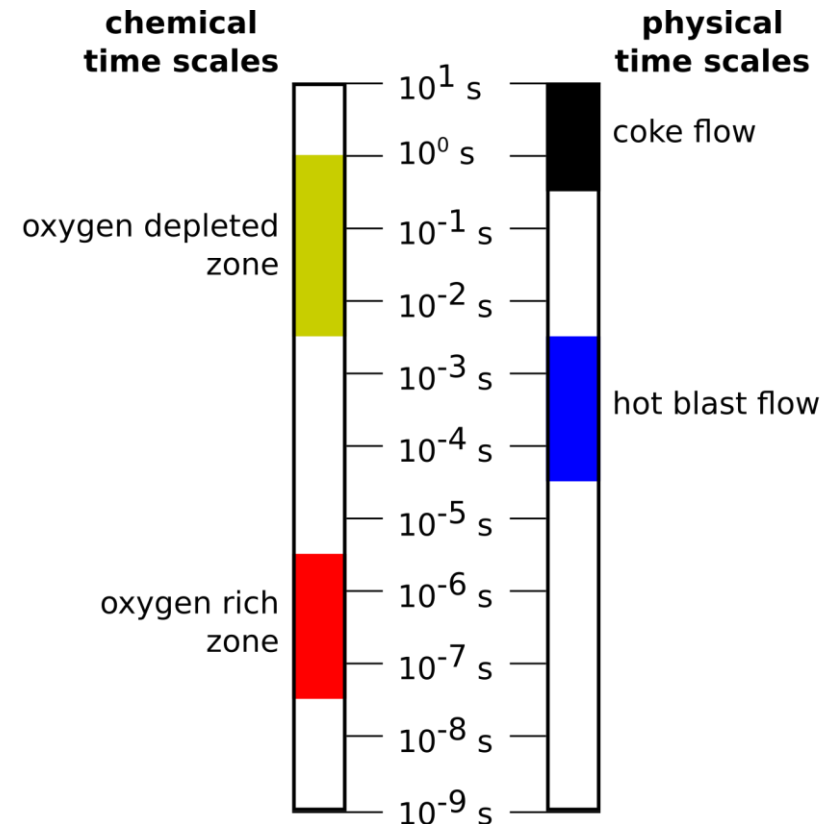


Chemical scales

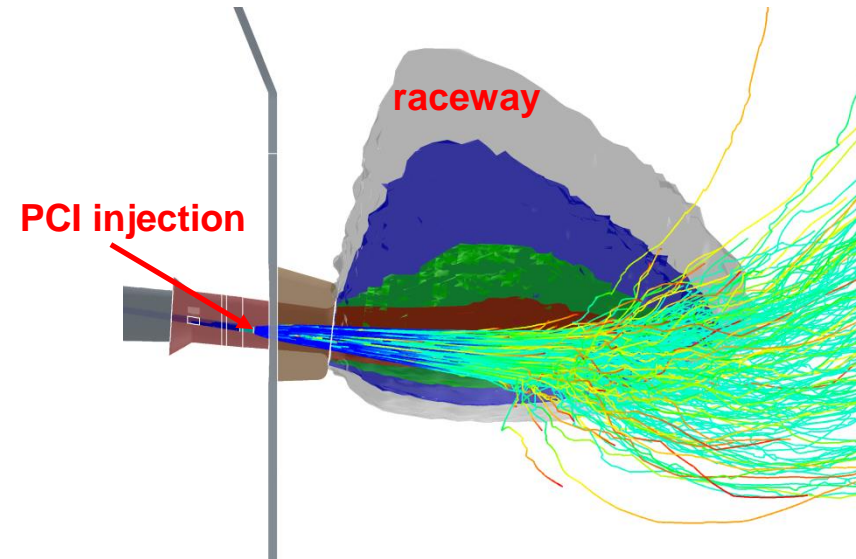
- ARA/coke conversion
- Gas-phase chemistry

Physical scales

- Gas/solid flow
- Turbulence
- Mass transport/transfer



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Fixed raceway shape based on literature, colors indicate porosity: 0.9 (red), 0.8 (green), 0.7 (blue), 0.6 (grey)¹

Temperature	Heating rates	Pressure	Relative velocity	Flow type	Residence time
1200 – 2500 K	$10^4 - 10^6$ K/s	2 – 5 bar _(a)	< 1- 100 m/s	Turbulent	< 100 ms

¹C. MAIER (2015): NUMERICAL MODELING OF THE BLAST FURNACE PROCESS – INJECTION OF AUXILIARY REDUCING AGENTS INTO THE RACEWAY, PHD THESIS, TU WIEN

²M. BÖSENHOFER ET AL. (2020): SUITABILITY OF PULVERISED COAL TESTING FACILITIES FOR BLAST FURNACE APPLICATIONS, IRONMAKING & STEELMAKING, VOL 47(5), PP. 574-585

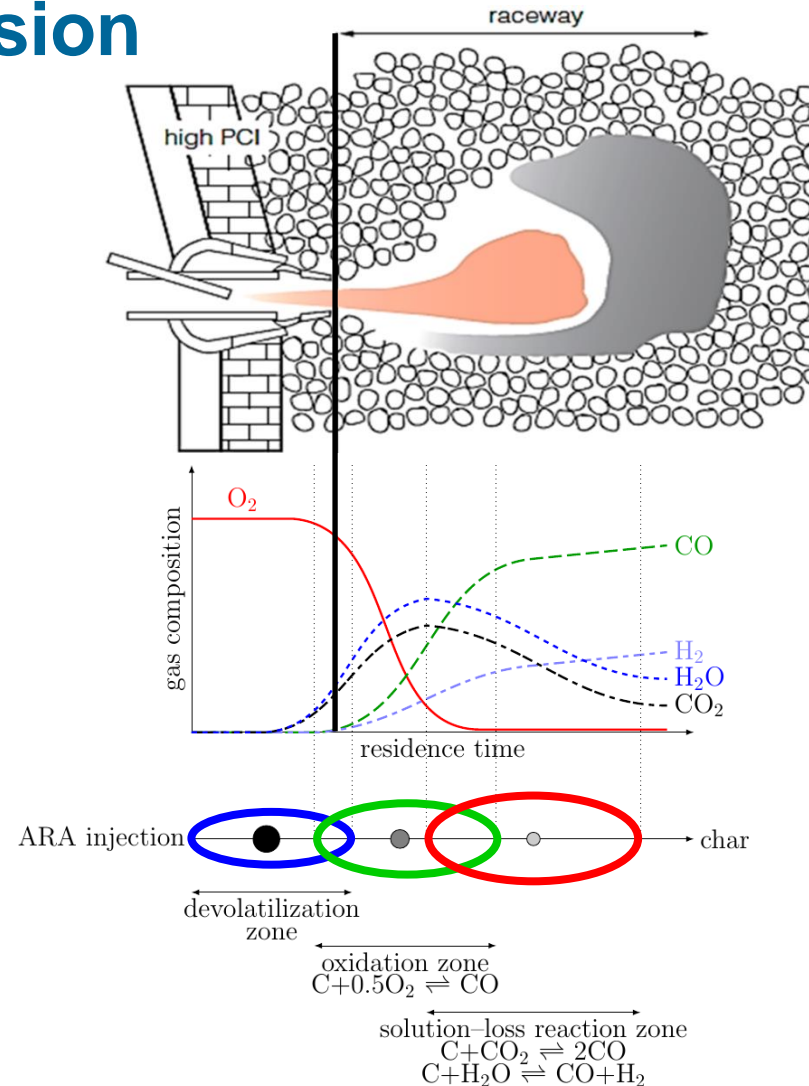
Thermochemical ARA conversion

What are ARAs?

- Pulverized carbon carriers
- Particle size: 10 μm – 10 mm

ARA conversion:

- Drying \rightarrow thermal or equilibrium
- Devolatilization \rightarrow single or two-step
- Oxidation \rightarrow diffusion limited
- Gasification \rightarrow diffusion limited



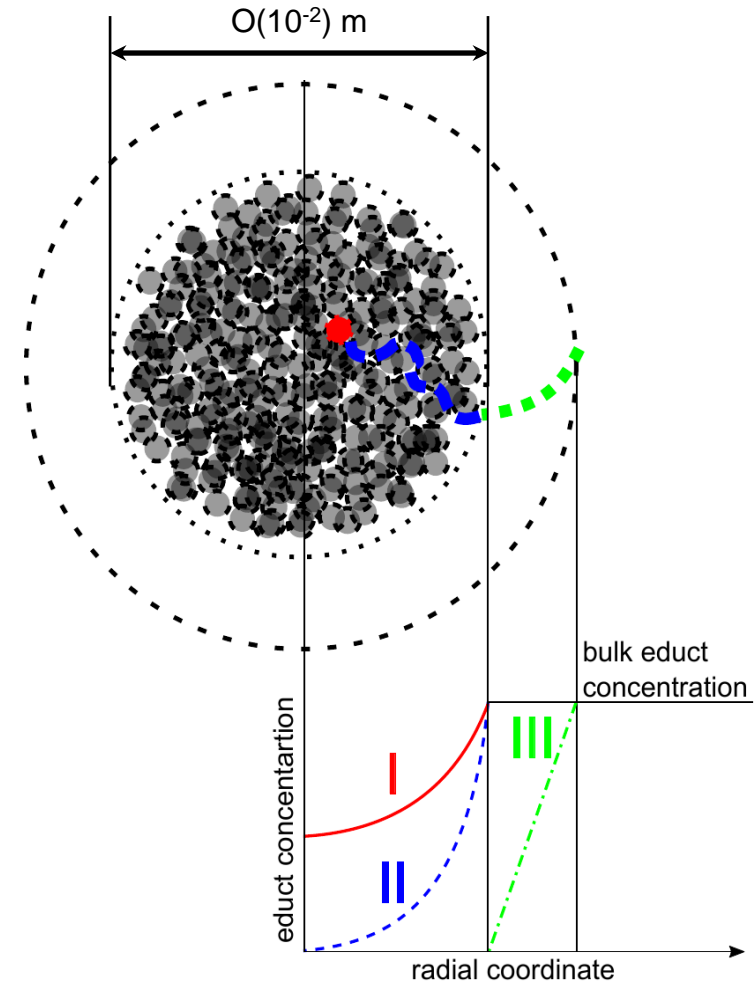
©T. KAMIJOU ET AL. (2000): PC COMBUSTION IN BLAST FURNACE. IN ADVANCED PULVERIZED COAL INJECTION TECHNOLOGY AND BLAST FURNACE OPERATION, VOLUME 1, PP. 63–82



Coke conversion:

- (Unreacted) progressive core
- Effective rate expression:

$$k_{eff,j} = \frac{1}{\frac{1}{k_{kin,j}} + \frac{1}{\eta_j}} + \frac{1}{h_{BL,j} A_{coke} C_j^{1-\nu}}$$



© M. BÖSENHOFER ET AL. (2019): MULTIPHASE REACTIVE SYSTEMS – ANALYSIS OF INVOLVED TIME SCALES, PROCEEDINGS: 9TH EUROPEAN COMBUSTION MEETING (ECM), 6 PAGES

Coke conversion:

- (Unreacted) progressive core
- Effective rate expression:

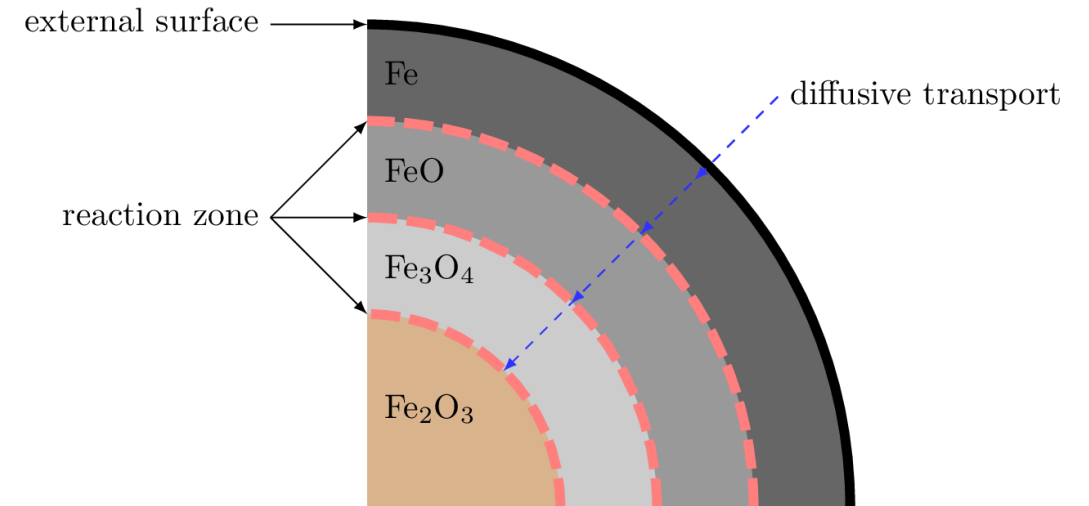
$$k_{eff,j} = \frac{1}{\frac{1}{k_{kin,j}} \cdot \eta_j} + \frac{1}{h_{BL,j} A_{coke} c_j^{1-\nu}}$$

Iron ore conversion:

- Unreacted shrinking core
- Effective rate expression:

$$\frac{1}{k_{eff,i}} = \frac{1}{A_s h_{m,i}} + \sum_{l>L} \left(\int_{r_{l+1}}^{r_l} \frac{dA}{D_{eff,i} A(r)} + \sum \frac{1}{k_{i,l}} \right) + \frac{1}{k_{i,L}}$$

$$k_{eq,i} = \left(k_{eff,i} + \frac{k_{eff,i}}{K_{eq}} \right) \cdot \left(c_i - \frac{c_j}{K_{eq}} \right)$$

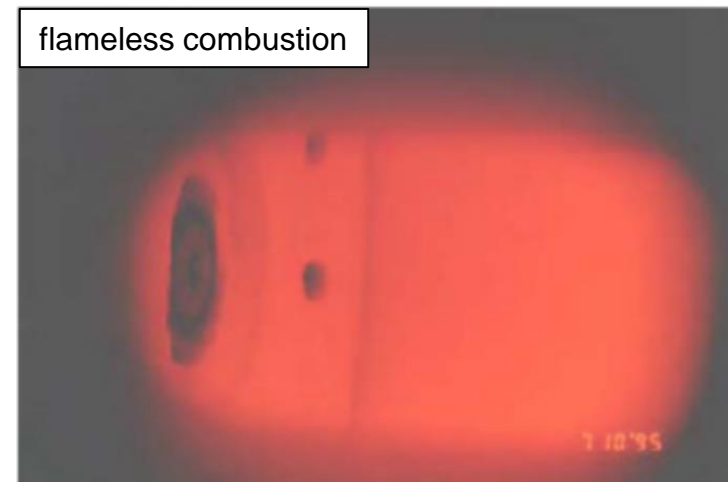
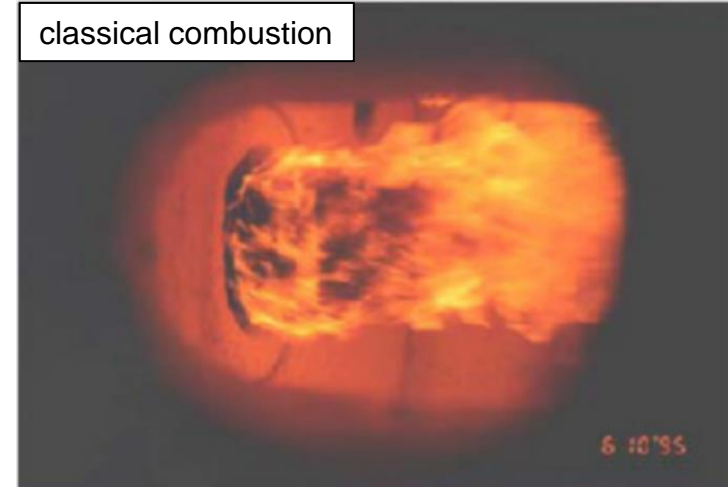


© M. BÖSENHOFER ET AL. (2023): AN EULERIAN-BASED REDUCTION MODEL FOR IRON ORE PARTICLE REDUCTION, AISTECH 2023, 8 PAGES

Gas-phase chemistry

Challenges:

- Different combustion regimes
- Multiple gas species sources (coke, ore, ARAs)
- Widely scattered characteristic scales
- Turbulence



© V. PANEBIANCO (2016): A NUMERICAL STUDY OF TURBULENCE-FLAME INTERACTION IN MILD COMBUSTION, PHD THESIS.

Gas-phase chemistry

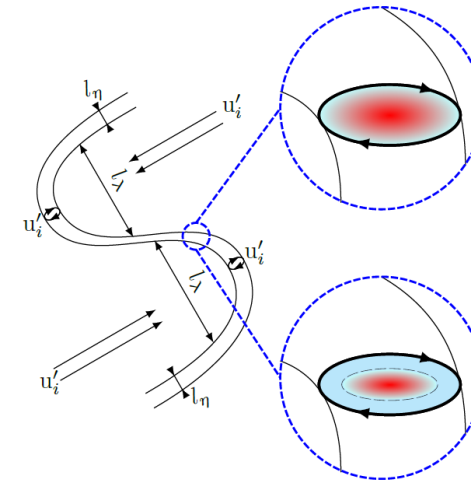
Challenges:

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Eddy Dissipation Concept (EDC):

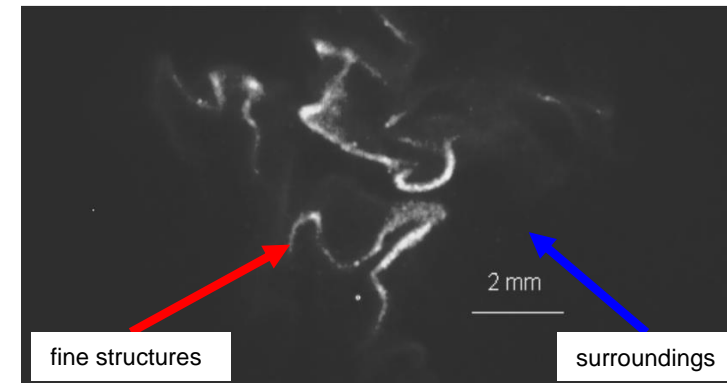
- Based on turbulence energy cascade
- Covers multiple regimes

classical combustion



flameless combustion

Comparison fine structures classical and MILD combustion.^{1,2}



Reacting structures of a premixed opposing jet flame.³

¹M. BÖSENHOFER ET AL. (2018): THE EDDY DISSIPATION CONCEPT—ANALYSIS OF DIFFERENT FINE STRUCTURE TREATMENTS FOR CLASSICAL COMBUSTION, ENERGIES 11(7):1902

²H. TENNEKES (1968): SIMPLE MODEL FOR THE SMALL-SCALE STRUCTURE OF TURBULENCE. THE PHYSICS OF FLUIDS, 11(3), PP. 669–671

³P. MAGNUSSEN (2009): INVESTIGATION INTO STRUCTURE AND BEHAVIOR OF LAMINAR AND TURBULENT FLAMES BY PLANAR LASER-INDUCED FLUORESCENCE MEASUREMENTS, PHD THESIS, NTNU

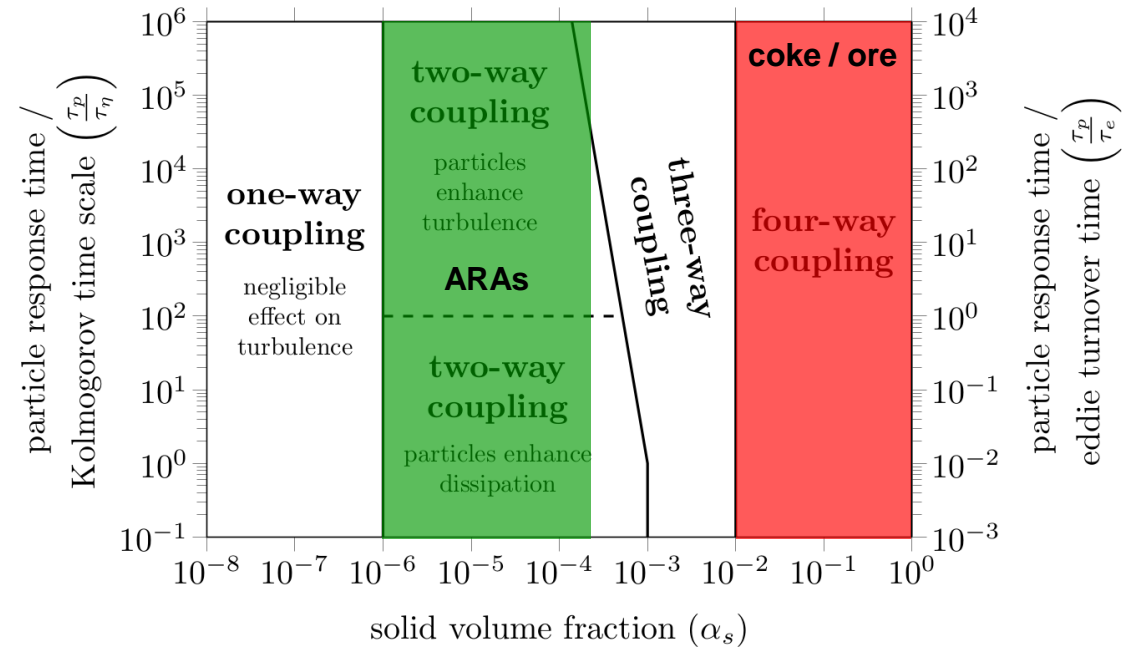


Involved phases:

- Gas
- Solid (coke, ore)
- Liquid (iron, slag)
- ARAs (pulverized solids)

Modeling strategy:

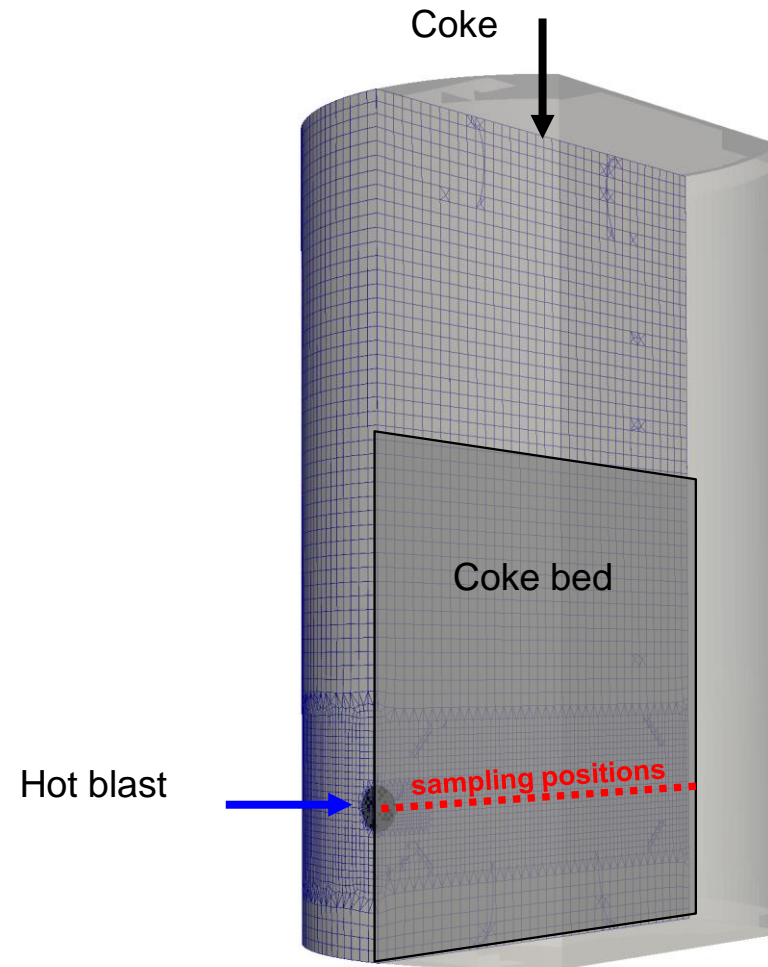
- Euler-Euler-Lagrange
- Continuous solid phases (KTGF)
- Point mass/1D Lagrangian ARA phases



© S. ELGHOBASHI (1994): ON PREDICTING PARTICLE-LADEN TURBULENT FLOWS, APPLIED SCIENTIFIC RESEARCH, VOL. 52, 309-329.

Lab-Scale blast furnace:

- Experimental raceway formation
- Measurement of species concentration in the raceway



Schematic illustration and mesh of the experimental setup from¹

¹ H. NOGAMI ET AL. (2004) RACEWAY DESIGN FOR THE INNOVATIVE BLAST FURNACE, ISIJ INTERNATIONAL 2004;44:2150–8

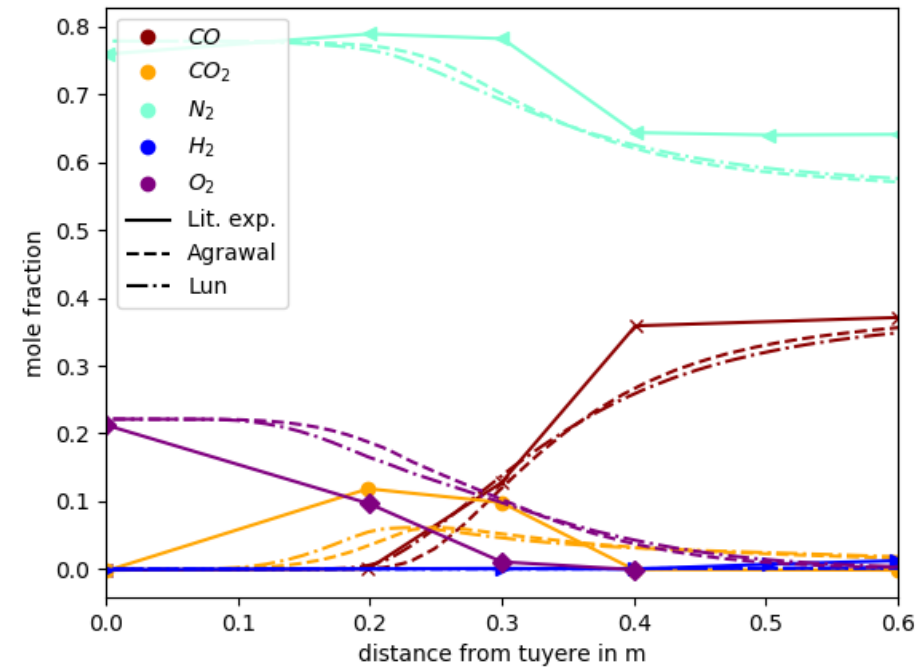


Lab-Scale blast furnace:

- Experimental raceway formation
- Measurement of species concentration in the raceway

Simulations results:

- No significant difference between KTGF closures
- Good agreement with experiments



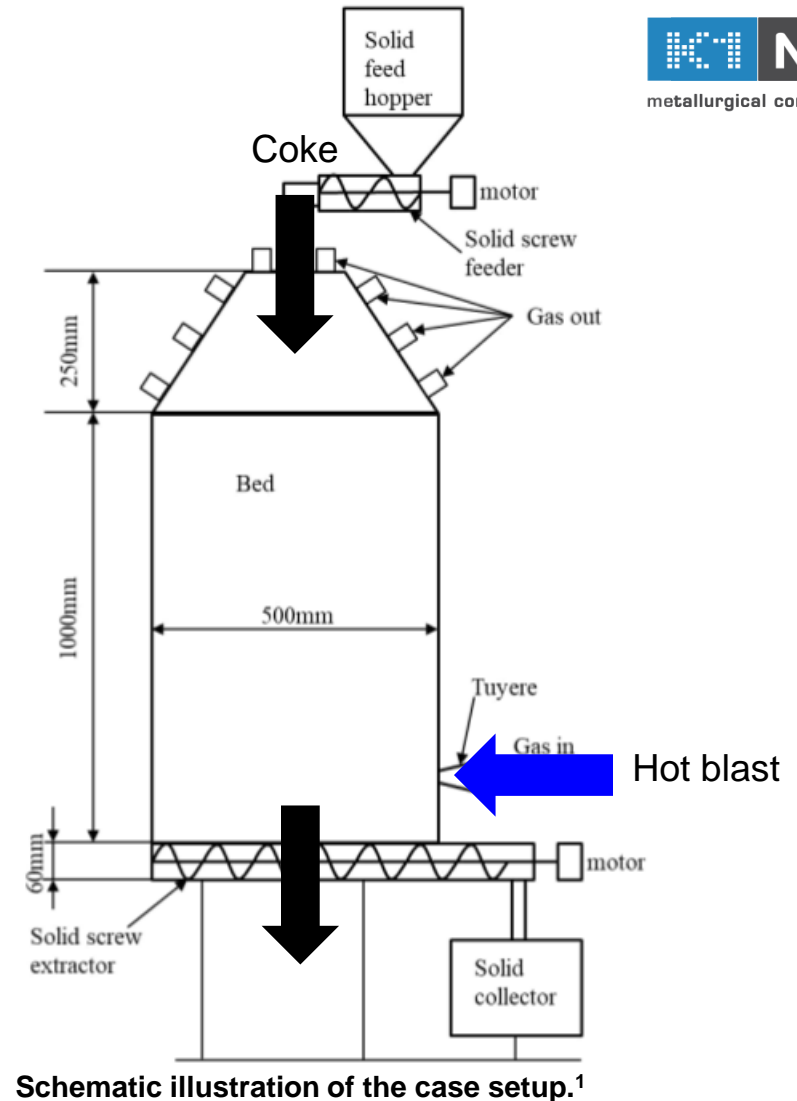
Comparison experimental and simulation result



Influence Coke :

- 2D experiments on raceway formation
- Continuous feeding from top
- Gas tight continuous discharging at bottom
- Varying coke conversion rates:

Case ID	Rate Variation
C0	$0 \cdot k_{\text{eff},i}$
C1	$0.5 \cdot k_{\text{eff},i}$
C2	$k_{\text{eff},i}$
C3	$100 \cdot k_{\text{eff},i}$



Schematic illustration of the case setup.¹

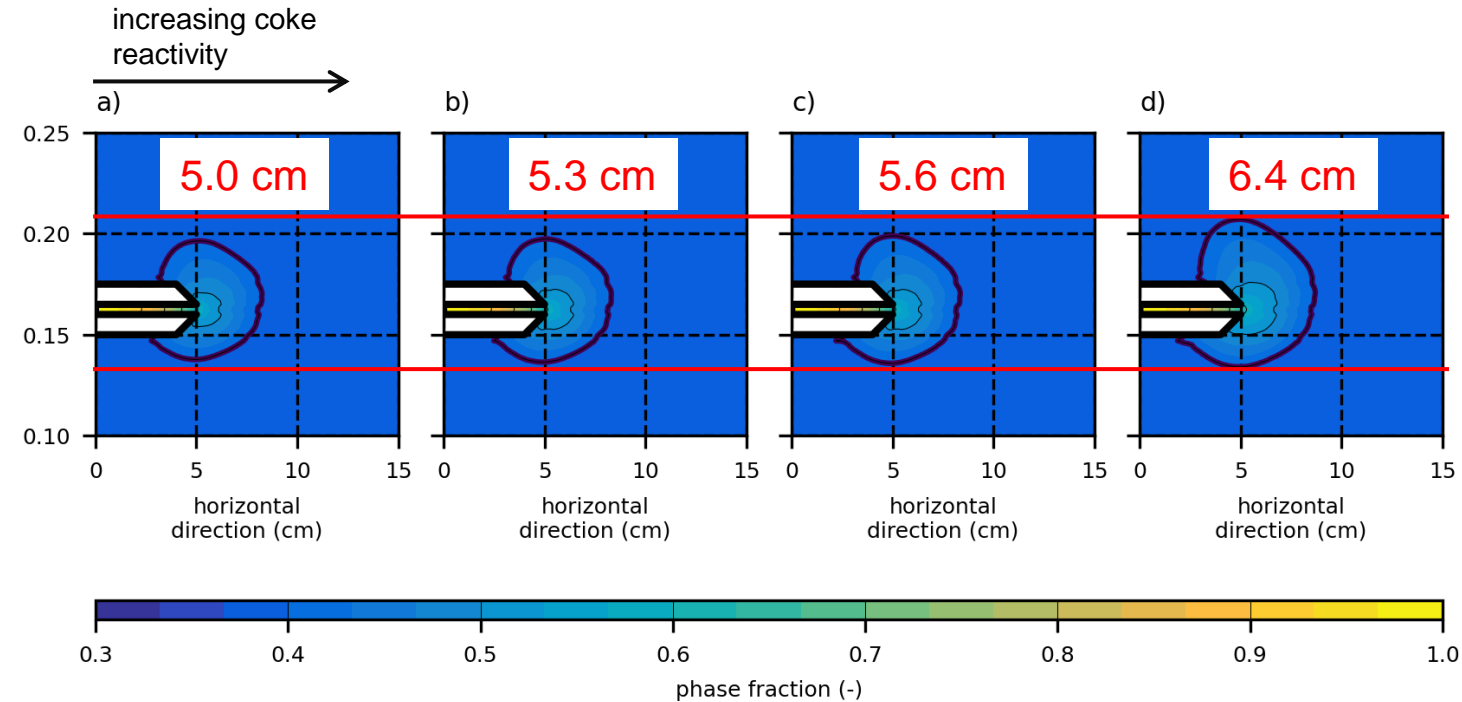
¹ V. MOJAMDAR, G.S. GUPTA, A. PUTHUKKUDI, RACEWAY FORMATION IN A MOVING BED, ISIJ INT. 58 (2018) 1396–1401.



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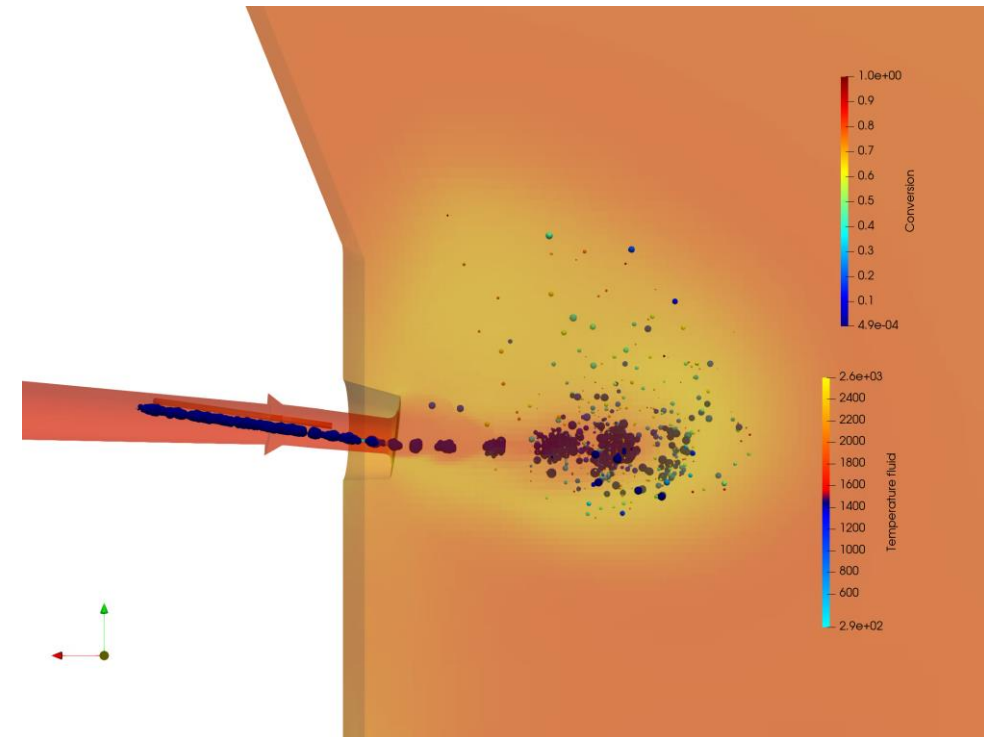
Hot blast phase fraction contours. a) C0; b) C1; c) C2; d) C3.



- Thermochemical raceway modeling complex:
 - Length/time scales
 - Multiple phases
 - Chemistry

- Comprehensive modeling framework
 - General multiphase reactors

- Investigation of blast furnace operation
 - ARA injection investigations
 - Coke consumption



Snapshot representative PCI injection simulation.

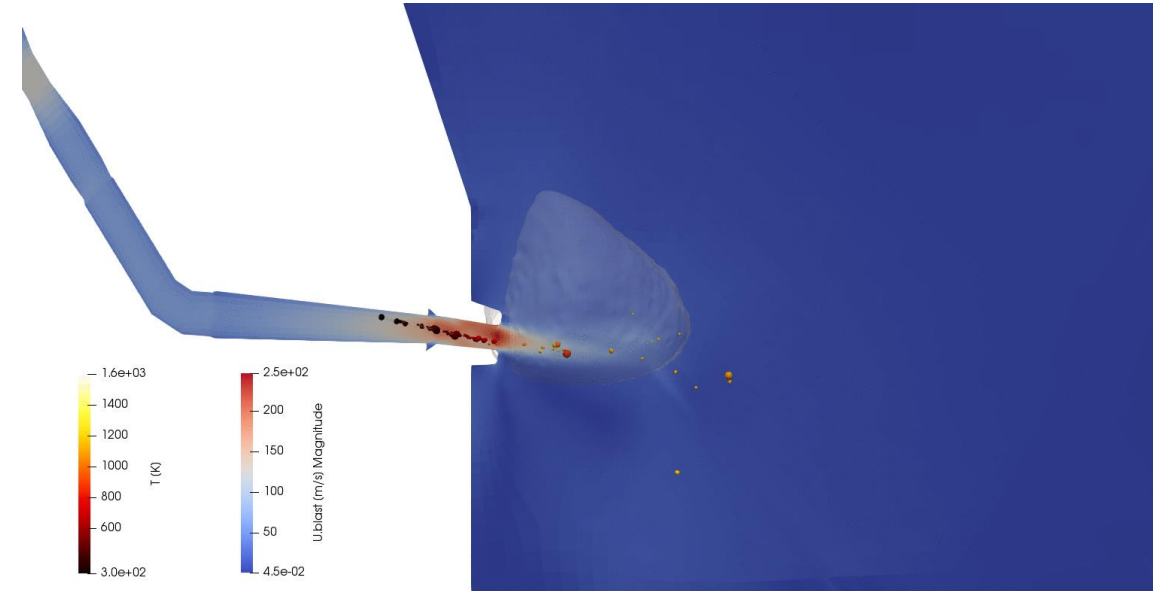
Kontakt

Markus Bösenhofer

Phone: +43 1 58801 166251

Email: markus.boesenhofer@tuwien.ac.at
markus.boesenhofer@k1-met.com

www.tuwien.at
www.k1-met.com



Snapshot representative PCI injection simulation.